Study of Incineration of Acacia Wood Chips for Biomass Power Plant of the Royal Thai Navy in Sattahip, Chonburi Province, Thailand

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Abstract—This research is aimed to find optimal values of parameters of acacia wood chips combustion in a bubbling fluidized bed for electrification within the area of the Royal Thai Navy in Sattahip, Chonburi province, Thailand. The size of wood chips falls in the range of 25 mm in diameter. The bed temperature is set within the range of 800±10°C with the air flow rate of 2.1-3.1 m/min corresponding to the air-fuel ratio between 0.71 and 1.03. The resulting thermal efficiency is approximately 95% with a thermal output of 474.76 kWh, which produced the electricity 0.131 kW-hr.

Keywords—Acacia Wood Chips, Biomass, Combustion, Fluidized Bed.

I. INTRODUCTION

BIOMASS is one of the most attractive sources for renewable energy and a promising alternative to fossil fuels due to the fact that biomass leads to the reduction in producing greenhouse gases and limiting the formation of pollution. Biomass fuels also contain low sulphur content thus low SOx emission. Thailand, as an agricultural country constantly provides varieties of biomass, especially from the agricultural and wood industry. Most of biomass has been used in direct combustion, which converts solid state of biomass into heat [1], for further small- to medium-sized electricity production in either in-house usage or consumption in rural areas. Acacia is one of the fast-growing crops found all over Thailand. It is considered as one of the potential main fuels in our small-scale biomass power plant for electrification within the navy area.

Fluidized bed technology has been extensively used in both combustion ([3]-[8], [10]) and gasification ([1], [9], [10]) due to its high efficiency in energy conversion from biomass. Bubbling fluidized bed and circulating fluidized bed combustors and gasifiers have been in attention of many researchers in the recent years. The first kind is attractive due to its capability of thorough mixing of fuel particles and air inside the bed; thus, the design of air distributor becomes crucial for the air inside the bed [6]. In spite of low NOx emission, both kinds of fluidized bed technologies experience high CO emission. Therefore, many researchers pay attention to this problem and have been striving to solve, e.g. employing air staging [4], which helps the circulating fluidized bed combustors reduce CO emission.

There are numerous attempts of studies of the combustion of wood chips in order to figure out properties of the material of biomass fuels themselves and heating values including the efficiencies of the combustion. Khan et al. [7] summarized the processes of wood chip combustion as follows, after heating wood, its constituents start to hydrolyze, oxidize, dehydrate and pyrolyse causing the elevated temperature and combustible volatiles, tar and reactive char. In addition, they presented the process in a detailed schematic chart describing a process at each temperature level. Han et al. [3] investigated both cypress pellets and sawdust, and found that despite the fact that the sawdust led to higher combustion efficiency and heating value [8], its combustion produced significant amount of unburned carbon and CO in its fly ash, and was difficult to operate at higher temperature than 650°C. Ammendola at al. [10] studied the effect of the mechanical strength on fuel particles of wood chips and pellets under combustion and gasification. They reported that the wood pellets confronted less fragmentation than the chips, but gave approximately 40% higher lower heating value and less moisture content. In addition, the attempts of pollutant reduction such as NO, CO, N2O and SOx caused by biomass combustion have been widely studied.

The objectives of this investigation is to figure out the optimum values of parameters related to the combustion of acacia wood chips in order to obtain high combustion efficiency and produce less pollutants. The studies parameters include feed air flow rate, ash content, size of the wood chips, and feed fuel flow rate. The chip moisture content is kept constant throughout the study.

II. EXPERIMENTAL PROCEDURE

A. Experimental Setup

Fig. 1 presents the schematic diagram of the bubbling fluidized bed system. The fluidized bed was made of a metal sheet of 6mm thickness, and was lined with refractory bricks.
and insulator bricks with the thickness of 0.25m. The combustion chamber was 2.5m in height with the insulated ceiling, and the air distributor was 10mm thick consisting of 12 nozzles and 4 bubble caps for feeding the fuel from underneath. The bed filled with silica sand was heated for start-up by a pilot burner using LPG. 12 type-K thermocouples connected with a digital thermometer readout were embedded in the combustor. The air supply system to the chamber consisted of the main duct connected with the blower and 3 spargers with globe valves. Each station of the fluidized bed system is described as follows. The screw feeder driven by a motor delivered the wood chips toward the combustor, where there was high velocity air flow through a nozzle injecting the chips down to the sand bed. This was to prevent the reverse air and fuel. Air was supplied to the fluidized bed combustor by two fans with different functions. A force draft fan was used to feed the air from underneath, and an induced draft fan for suction of the air on the top of the fluidized bed combustor. Fly ash as a product of combustion was collected at the exit of the cyclone.

Fig. 1 Schematic diagram of experimental set-up

### B. Experimental Procedure

Throughout the research, experiments were repeated 5 times for the statistical reliability, and the average as well as the standard deviation was reported. The sundried acacia wood chips with 19% moisture of 25mm diameter were put in each bag of 500g in order to record the amount of the fuel particles as rate was set by adjusting glove valves at the air supply pipes and time fed to the fluidized bed combustor. Then, the air flow chips with 19% moisture of 25mm diameter were put in each standard deviation was reported. The sundried acacia wood for the statistical reliability, and the average as well as the

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Carried out in order to calculate the thermal efficiency of the combustion as shown below:

\[ \eta = \frac{(Q_{in} - Q_{ash} - Q_{CO}) \times 100}{Q_{in}} \]  

where \( \eta \) represents combustion efficiency in percentage. \( Q_{in} \) is the input heat to the combustion system, kJ, obtained from the heat of combustion of the acacia wood chips with 19% moisture plus the heat of hot feed air. \( Q_{ash} \) is heating value of the fly ash obtained from the combustion, kJ. \( Q_{CO} \) is the heating value of carbon monoxide, kJ.

### III. RESULTS AND DISCUSSION

Table II reports the average values of constituents contained in the exhaust gas at 380°C. The heating value of the fly ash is quite high, and was thought to be used as a recovery energy in the future work. The concentration of \( \text{SO}_2 \) was quite low; however, \( \text{CO} \) content was found higher than the benchmark for the lab scale fluidized bed of approximately 800ppm [6]. This problem is left for our future research focusing on the \( \text{CO} \) and \( \text{NO}_x \) emission control. In addition, in this study, \( \text{NO}_x \) emission was expected to be quite acceptably low. This was probably because the bubbling fluidized bed operated at the temperature lower than 1300 K, at which \( \text{N}_2 \) and \( \text{O}_2 \) were dissociated and formed \( \text{NO} \).

More detailed information from Table II is to be discussed in the following sections.

### A. Heating Value

The ash heating value decreased with the air flow rate as displayed in Fig. 2. The relationship shows a spline trend line of a very good curve fit with \( R^2 \) of 0.993. This could be explained by the fact that as the flow rate was increased, the particle fuels inside the bed was vigorously stirred, and thoroughly mixed. Furthermore, the more amount of air increased the chance for the particles to contact with the air.
leading to better burning. Increasing air flow also enhanced the continuous combustion with the ash above the bed, and this caused the drop of the heating value. This was because increasing the air flow caused the hot air temperature to become equal to the bed one, and the higher bed temperature gave rise to better ash combustion; thus the heating value was reduced.

![Graph showing the relationship between air flow rate and ash heating value.](image)

**Fig. 2 Relationship between air flow rate and ash heating value**

### B. Combustion Efficiency

With a fixed bed temperature of 800°C, the combustion efficiency was increased linearly with the air flow rate as shown in Fig. 3. This was due to the fact that the sand moved aggressively allowing oxygen to be more in contact with the wood chips leading to better reaction. Nonetheless, feeding too much air may affect the efficiency, because there would be more bed voidage leading to less contact area between the biomass particles and oxygen. Therefore, within this research, the feed air was slightly deficient (see Table I).

![Graph showing the relationship between thermal efficiency and air flow rate.](image)

**Fig. 3 Linear relationship between thermal efficiency and air flow rate**

### C. Analysis of Exhaust Gas

Fig. 4 shows the distributions of flue gas emissions in different air flow rates. The trend lines of concentrations of CO₂, CO and SO₂ are similar viz., increasing the air flow rate reduced their concentrations, especially for SO₂, when the flow rate was greater than 0.004659 m³/s, its concentration went towards zero. This could be explained by the fact that higher air flow rate, in other words, higher O₂ concentration, and helped better combustion. However, the trend lines of concentration of O₂ and N₂ shows similarity, because as the air flow rate was increased to 0.005065 m³/s, their concentrations was decreased, then they remained nearly constant when the flow rate lay between 0.005065 and 0.005875 m³/s. Finally, for the flow rate greater than 0.005875 m³/s, the concentrations soared. This was simply explained by some values in Table III such as air-fuel ratio (A/F ratio) showing the air deficiency for the flow rates between 0.004254 and 0.005875 m³/s, whereas at 0.006280 m³/s the excess air played important role.

![Graph showing the exhaust gas constituents at different air flow rates.](image)

**Fig. 4 Exhaust gas constituents at different air flow rates**

### TABLE III

<table>
<thead>
<tr>
<th>Condition</th>
<th>Test No.</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>2</td>
</tr>
<tr>
<td>Air flow rate m³/s</td>
<td>0.00425</td>
</tr>
<tr>
<td>A/F Ratio -</td>
<td>0.71:1</td>
</tr>
<tr>
<td>O₂ Content % V</td>
<td>14.9</td>
</tr>
<tr>
<td>CO₂ content ppm</td>
<td>1,203.0</td>
</tr>
<tr>
<td>CO content ppm</td>
<td>1,203.0</td>
</tr>
<tr>
<td>N₂ content % V</td>
<td>56.05</td>
</tr>
<tr>
<td>SO₂ content ppm</td>
<td>40</td>
</tr>
</tbody>
</table>

### IV. CONCLUSIONS

The combustion of acacia wood chips of 19% moisture content was carried out in a bubbling fluidized bed with fluidized velocity of 0.65m/s. The combustion efficiencies in all cases were higher than 94%, whereas the ash heating values were high enough to be thought for recovery in the future work. Flue gas was analyzed and found that the concentration of carbon monoxide was higher than the benchmark of 800ppm; hence, the problem of CO reduction was left to our future research, whereas the concentration of sulphur dioxide was touching zero. The combustion produced 474.76 kWth and electricity of 0.131 kW-hr. This can be concluded that the acacia wood chip combustion in the bubbling fluidized bed has high potential for being a renewable energy source for the Royal Thai Navy in Sattahip, Chonburi province, Thailand.
REFERENCES


