A Kinetic Study on the Adsorption of Cd(II) and Zn(II) Ions from Aqueous Solutions on Zeolite NaA

Dimitar Georgiev, Bogdan Bogdanov, Irena Markovska, Yancho Hristov and Dencho Stanev

Abstract—The present paper reports the removal of Cd(II) and Zn(II) ions using synthetic Zeolite NaA. The adsorption capacity of the sorbent (Zeolite NaA) strongly depends on simultaneous or not simultaneous (concurrent) presence of Cd(II) and Zn(II) in the sorbate. When Cd(II) and Zn(II) are present simultaneously (concurrently) in the sorbate, Zn(II) ions were sorbed at higher rate. Equilibrium data fitted Langmuir, Freundlich and Tempkin isotherms well. The applicability of the isotherm equation to describe the adsorption process was judged by the correlation coefficients R². The Langmuir model yielded the best fit with R² values equal to or higher than 0.970, as compared to the Freundlich and Tempkin models. The fact that 1/n values range from 0.322 to 0.755 indicates that the adsorption of Cd(II) and Zn(II) ions from aqueous solutions also favored by the Freundlich model.

Keywords—Adsorption, adsorption capacity, kinetic sorption, Zeolite NaA

I. INTRODUCTION

The properties of drinking waters and these used in food industry, as well as waters packed for retail selling should conform to certain requirements regarding their contents of chemical compounds like nitrates, phosphates, heavy metals, etc. One method for removal of heavy metals from drinking water is treatment with synthetic zeolites.

Using zeolites as sorbents is preferred due to their specific structure allowing selectivity of the processes involved (adsorption and ion-exchange), simple operation and effectiveness. This is achieved as a result of the main properties of synthetic zeolites like highly developed porous surface, phase purity and resistance to chemical reagents.

The present paper deals with issues referred to studies on the possibility to purify aqueous solutions containing cadmium and zinc ions using synthetic zeolite NaA with the methods of adsorption and ion-exchange. Cadmium and zinc ions are hazardous components in drinking waters even at low concentrations (maximum allowable concentration of Cd(II) is 0.005 mg/dm³) [1]-[4]. Higher levels of Cd(II), as well as other heavy metals, in water facilities poses great risk to human health. Therefore, it is of major importance to find ways for lowering concentration or removing such contaminants from basins used for drinking water [5],[6].

For this purpose, the paper discusses the adsorption kinetics of synthetic zeolite NaA in model aqueous solutions containing cadmium and zinc ions, as well as the various factors affecting the process of adsorption. The results obtained are further adapted in kinetic models and an assessment of the adsorption processes is made.

II. MATERIALS AND METHODS

A. Adsorbate

All the compounds used to prepare the reagent solutions were of analytic reagent grade. The initial cadmium and zinc solutions were prepared from deionized water and Cd(NO3)2·4H2O and ZnSO4 (Merck).

B. Adsorbent

The adsorbent used for the studies was synthetic zeolite NaA produced from kaolin of Bulgarian origin by a technology described earlier [7],[8].

C. Batch Adsorption Studies

The adsorption of Cd(II) and Zn(II) ions from model aqueous solutions by the zeolite NaA studied was performed with different initial concentrations and constant temperature (20°C).

The adsorption kinetics was studied by the method of voltamperometric, using volt-amperometer ECOTEST-VA (ECONIX-EXSPERT). This method allows direct registration of the amount of Cd(II) and Zn(II) in the adsorbate monitored at every moment of contact with the adsorbent (zeolite NaA) [9].

The measuring system was specially designed for the experiments to allow constant homogenization (at varied propeller velocities) for better contact between adsorbent and adsorbate, as well as to provide possibilities for isothermal periods in thermostatic cell.

First, certain amount of cadmium and zinc salts were added step-wise under continuous propelling to plot the concentration curve. Then the adsorbent was added (Zeolite NaA – 20mg) and, after a period of time, measurements of the residual amounts (non-adsorbed) of the ions studied were started. pH of the system was in the range 3-5 since the method requires addition of HCl and Hg(NO3)2·H2O. Fig.1 shows the working...
voltage-current curves for the strides of the adsorption in model solutions containing: (a) Cd(II) ions only, (b) Zn(II) ions only and (c) both Cd(II) and Zn(II) ions.

As can be seen from the voltage-current plots, the Cd(II) ions were registered at voltages about 1600 mV, Zn(II) ions at about 1900-1100 mV, and certain amounts of Hg(II) ions were observed at about 200 mV. The amounts of these ions were calculated by the area of the peaks recorded. The method is quite sensitive because it allows registration of very small quantities of metal ions.

D. Adsorption Isotherms

To study the kinetics of adsorption, 100 ml model solution of Cd(II), Zn(II) and Cd(II)+Zn(II) (together) with initial concentration of 2 or 15 mg/L were placed in flat-bottomed flask (under continuous agitation and the constant temperature selected). By the mixing with the adsorbent, the decrease of the amount of the ions studied was monitored and recorded for a period of 30 min.

The adsorption capacity of the sorbent \(q_e\), mg/g was calculated by (1).

\[
q_e = \frac{(C_o - C_e)V}{m}
\]  

Where \(C_o\) and \(C_e\) are initial and final sample concentrations (mg/l) respectively, \(V\) are the volume of the sample solution and \(m\) is the weight of adsorbent added.

III. RESULTS AND DISCUSSION

A. Isotherm Data Analysis

The parameters obtained from the different models provide important information on the adsorption mechanisms and the surface properties and affinities of the adsorbent. The most widely accepted surface adsorption models for single-solute systems are the Langmuir and Freundlich models. The correlation with the amount of adsorption and the liquid-phase concentration was tested with the Langmuir, Freundlich and Tempkin isotherm equations. Linear regression is frequently used to determine the best-fitting isotherm, and the applicability of isotherm equations is compared by judging the correlation coefficients.

Fig.2 shows the adsorption kinetic isotherms from 100 ml model solution of Cd(II), Zn(II) and Cd(II)+Zn(II) (together).
\[ C_e = \frac{1}{q_e} K_c q_m + C_e \] (2)

Where \( q_e \) is adsorption capacity at equilibrium (mg/g), \( q_m \) is the maximum adsorption capacity (mg/g), \( C_e \) (mg/l) is the solution concentration at equilibrium, and \( K_c \) is the Langmuir constant (l/mg) [10]-[14].

2. Freundlich Isotherm

The linear form equation of the Freundlich isotherm is listed as follows:

\[ \log q_e = \log K_f + \frac{1}{n} \log C_e \] (3)

Where \( q_e \) is adsorption capacity at equilibrium (mg/g), \( C_e \) is the concentration at equilibrium (mg/l), \( K_f \) and \( n \) are the Freundlich constants. The value of \( K_c \) can be taken as a relative indicator of adsorption capacity while \( 1/n \) is indicative of the energy or intensity of reaction. The values of \( q_{max}, K_f \), \( K_f \) and \( n \) (3) are calculated from the intercepts and slopes of the equation plots.

3. Temkin Isotherm

Temkin isotherm, which considers the effects of the heat of adsorption of all molecules in the layer would decrease linearly with coverage due to the adsorbate and adsorbent interactions and is given by:

\[ q_e = \left(\frac{RT}{b}\right) \ln A + \left(\frac{RT}{b}\right) \ln C_e \] (4)

Here \( RT/b = B \) (J mol\(^{-1}\)), which is Temkin constant related to heat of sorption whereas \( A \) (L g\(^{-1}\)) is the equilibrium binding constant corresponding to the maximum binding energy. \( R \) (8.314, J mol\(^{-1}\) K\(^{-1}\)) is universal gas constant and Temperature (K) is absolute solution temperature.

The kinetic parameters, which are helpful for the prediction of adsorption rate, give important information for designing and modeling the adsorption processes.

<table>
<thead>
<tr>
<th>Isotherm model parameters</th>
<th>Cd(II)</th>
<th>Zn(II)</th>
<th>Cd(II), (together)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Langmuir qₘ</td>
<td>maximum monolayer adsorption capacities, mg/g</td>
<td>2.347</td>
<td>4.587</td>
</tr>
<tr>
<td>Kₗ - Langmuir constant, L/mg</td>
<td>3.952</td>
<td>0.719</td>
<td>2.272</td>
</tr>
<tr>
<td>R² - Correlation coefficient</td>
<td>0.9733</td>
<td>0.9855</td>
<td>0.9995</td>
</tr>
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<td>Freundlich 1/n - Freundlich exponent</td>
<td>0.322</td>
<td>0.554</td>
<td>0.588</td>
</tr>
<tr>
<td>Kᵣ - Affinity Factor, mg/g</td>
<td>9.275</td>
<td>7.335</td>
<td>4.335</td>
</tr>
<tr>
<td>R² - Correlation coefficient</td>
<td>0.8259</td>
<td>0.7723</td>
<td>0.8155</td>
</tr>
<tr>
<td>Temkin Kₚ - Temkin constant, L/g</td>
<td>6.960</td>
<td>5.443</td>
<td></td>
</tr>
<tr>
<td>B, J/mol</td>
<td>5.050</td>
<td>2.437</td>
<td></td>
</tr>
<tr>
<td>R² - Correlation coefficient</td>
<td>0.9775</td>
<td>0.9184</td>
<td></td>
</tr>
</tbody>
</table>

1. Pseudo-first-order Model

The adsorption kinetic data were described by the Lagergren pseudo-first-order model, which is the earliest known equation describing the adsorption rate based on the adsorption capacity. The equation for linear form is:

\[ \log(q_e - q_t) = \log q_e - \frac{k_1 t}{2.303} \] (5)

where \( q_t \) and \( q_e \) are the adsorption capacity at equilibrium and at time \( t \), respectively (mg g\(^{-1}\)), \( k_1 \) is the rate constant of pseudo-first-order adsorption (L min\(^{-1}\)).

2. Pseudo-second-order Model

The adsorption kinetic may be described by the pseudo-second-order model.

The equation for linear form is:

\[ \frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \] (6)

Where \( q_t \) and \( q_e \) are ion of heavy metal per mass unit of adsorbent (mg/g) at equilibrium and specific times, \( k_2 \) (g/mg min) are the rate constants of the second order kinetics.

The initial sorption rate, \( h \), can be defined as \( h=K_q q_e^2 \) so (6) can become:

\[ q_t = \frac{t}{\left(\frac{1}{h} + \frac{t}{q_e}\right)} \] (7)

Fig. 3 Tempkin plot for Cd(II)+Zn(II) (together) ions adsorption onto Zeolite NaA

Fig. 4 Pseudo-first-order kinetics for Cd(II)+Zn(II) ions (together) adsorption onto Zeolite NaA. Conditions: adsorbent 0.02 g/100 ml, pH 3-5, temperature 20 ± 2 °C

Fig. 2 Second order kinetics for Cd(II)+Zn(II) ions (together) adsorption onto Zeolite NaA. Conditions: adsorbent 0.02 g/100 ml, pH 3-5, temperature 20 ± 2 °C
The initial sorption rate, \( h \) (mmol \( \cdot \) g\(^{-1}\) min\(^{-1}\)), the equilibrium sorption capacity, \( q_e \), and the pseudo-second-order rate constant, \( k_2 \), can be determined experimentally from slope and intercept of plotting of \( t/q_t \) against \( t \).

IV. CONCLUSION

In this study, the kinetic sorption of Cd(II), Zn(II) were investigated and the following conclusions can be obtained. The adsorption capacity of the sorbent (Zeolite NaA) strongly depends on simultaneous or not simultaneous (concurrent) presence of Cd(II) and Zn(II) in the sorbate. When Cd(II) and Zn(II) are present simultaneously (concurrent) in the sorbate, Zn(II) ions were sorbed at higher rate. The adsorption capacity of the metal ions were found to be strongly dependent on pH. Complete adsorption for Cd(II), Zn(II) ions was achieved at pH 3-5. The removal mechanism of the metal ions was mainly by adsorption and ion exchange processes. The Langmuir model have been proved as suitable model explaining the phenomena of adsorption isotherm.

ACKNOWLEDGMENT

The financial support of the Ministry of Education and Sciences (National Science Fund), Bulgaria, is gratefully acknowledged!