PI Controller for Automatic Generation Control
Based on Performance Indices

Kalyan Chatterjee¹

Abstract—The optimal design of PI controller for Automatic Generation Control in two area is presented in this paper. The concept of Dual mode control is applied in the PI controller, such that the proportional mode is made active when the rating of change of the error is sufficiently larger than a specified limit otherwise switched to the integral mode. A digital simulation is used in conjunction with the Hooke-Jeeve’s optimization technique to determine the optimum parameters (individual gain of proportional and integral controller) of the PI controller. Integrated Square of the Error (ISE), Integrated Time multiplied by Absolute Error (ITAE), and Integrated Absolute Error (IAE) performance indices are considered to measure the appropriateness of the designed controller. The proposed controller is tested for a two area single nonheat thermal system considering the practical aspect of the problem such as Deadband and Generation Rate Constraint (GRC). Simulation results show that dual mode with optimized values of the gains improved the control performance than the commonly used Variable Structure.

Keywords—Load Frequency Control, Area Control Error (ACE), Dual Mode PI Controller, Performance Index,

I. INTRODUCTION

The analysis and design of Automatic Generation Control (AGC) system of individual generators eventually controlling large interconnections between different control areas play a vital role in automation of power system. The sensitivity of any power plant depends upon the response time taken by the automatic generation controller to take care of the frequency change. The purposes of AGC are to maintain system frequency very close to a specified nominal value, to maintain generation of individual unit at the most economic value, to keep the correct value of the line power between different control areas. If the load is increased, AGC system increases the mechanical torque by increasing the steam flow rate to compensate the load by increasing the generator’s output economically in an area. This process must be repeated constantly on a power system because the load changes constantly. The conventional control strategy for the AGC problem is to take the integral of the control error as the control signal. By the way of using integral controller, zero steady-state frequency deviation can be achieved but the dynamic performance of such controllers is unsatisfactory. Variable structure concept has been used by some of the investigators [1-3] to cope with the Load Frequency Control (LFC) problem. The concept of dual-mode control is applied in the PI controller such that the proportional mode is made active when the rate of change of the error is sufficiently larger than a specified limit otherwise switched to the integral mode. A digital simulation is used in conjunction with the Hooke-Jeeve’s optimization technique to determine the optimum parameters (individual gain of proportional and integral controller) of the PI controller. Three different types of performance indices are considered to measure the appropriateness of the designed controller. The concept of dual mode with optimized values of the gains improves the performance of the controller and reduces the overshoot and settling time of the system response.

II. ANALYSIS IN THE TIME DOMAIN

The design of linear control systems can be carried out in either the time or the frequency domain. Design in the time domain using performance specifications as rise time, delay time, settling time, maximum overshoot and so on, is feasible analytically only for second order systems or systems that can be approximated by second order systems. General design procedures using time - domain specifications are difficult to establish for systems with order higher than the second. But, the development and availability of high - powered and user-friendly computer software is rapidly changing the practice of control system design. With modern computer software tools, the designer can go through a large number of design runs using the time-domain specifications within a matter of minutes. This considerably diminishes the historical edge of the frequency- domain design, which is based on the convenience of performing graphical design manually. In addition, it is generally difficult, except for the experienced, to select a meaningful set of frequency- domain specifications that will correspond to the desired time domain performance requirements. In this work, the secondary controller is designed in time domain specifications.

III. TWO-AREA WITH INTEGRAL CONTROLLER

The guiding principle in pool operation is that each area in normal steady state should supply its own load and such portions of other areas load as had been agreed upon. It is required that the steady-state tie-line power deviation following load changes must be brought to zero. For making the steady state error zero, integral controller is used as a supplementary controller.

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Fig. 1 Complete Block Diagram of Two-Area System with Integral Controller

From this Fig.1 the command signals \( P_{C_i} (i = 1, 2) \) will be of the form

\[
\Delta P_{d1} = -\kappa_1 \left( \Delta P_{12} + B_1 \Delta f_1 \right) k t
\]

\[
\Delta P_{c2} = -\kappa_2 \left( \Delta P_{21} + B_2 \Delta f_2 \right) k t
\]

The constant \( \kappa_1 \) and \( \kappa_2 \) are integrator gains, and the constants \( B_1 \) and \( B_2 \) are the frequency bias settings. The type of control is known as the tie-line bias control. The static response of the system shows that the steady state frequency response and tie line power deviation can be eliminated with integral controller.

IV. THE PI CONTROLLER

One of the most widely used control laws in thermal power station governing systems is the PI type controller. Proportional controller is used to reach the steady state condition much quicker because of the faster transient response with proportional controller. The proportional term of the controller produces a control signal proportional to the error in the system, so that \( u(t) = \kappa_P e(t) \). Typically, given a step change of load demand, low values of \( \kappa_P \) give rise to stable responses with large steady-state errors. Higher values of \( \kappa_P \) give better steady-state performance, but worse transient response. Therefore, the higher value of \( \kappa_P \) is used to reduce the steady state error, although increasing the gain \( \kappa_P \) decreases the system time constant and damping. Therefore it is evident to choose the optimum value of \( \kappa_P \).

The proportional action can never eliminate the steady state error in the system because some (small) error must be present in order to produce a control output. A common way of reducing the steady state error is by incorporating integral action into the controller. Here, the control signal generated is proportional to the integral of the error signal, that is \( u(t) = \kappa_I \int e(t) dt \), where \( \kappa_I \) is the integral gain. While an error exists, the integrator tends to increase control action, thus driving the plant output towards the demand output. Then, when the error disappears, the continuing integrator output can be used to maintain the control action necessary for steady-state conditions. But, if the gain of integrator \( \kappa_I \) is sufficiently high, overshoot will occur increasing sharply as a function of the gain, this is highly undesirable. Lower value of \( \kappa_I \) reduce overshoot but increase rise time of the system. Based upon discussion it is required to design both the \( \kappa_P \) and \( \kappa_I \) properly.

It is well known that if the control law employs integral control the system has no steady state error. However, it increases the type of system by one. Therefore, the response with the integral control is slow during the transient period as shown in Fig.2. In the absence of the integral control when only proportional controller will act, gain of closed loop system can be increased significantly thereby improving the transient response. Therefore, the system reaches steady state much quicker because of the faster transient response. This can be observed from the response with proportional controller in Fig.2. However, the disadvantage with the proportional controller is that the system displays a steady state error. From these studies, one may draw the conclusion that the control law should be based on a compromise between the proportional and integral controller. The result of this compromise is also given in Fig.2 for the case of the PI control. It is seen that with the integral control system approaches steady state at a faster rate than with the PI control. It means that PI compromise does not eliminate the conflict between the static and dynamic performance of the system. The PI control strategy has slightly smaller deviation at the first peak than integral control strategy but settling time for only integral control is less. Also the response with the PI controller is more oscillatory than the integral controller [6].

Based upon the above-mentioned facts, it is desirable to introduce a dual concept involving both proportional and integral controller. The proportional controller will act during the transient period when rate of change of the error is sufficiently larger, whereas the integral controller would be the better option when the rate of change of the error is small.

V. THE PROPOSED APPROACH

The structure of the Dual Mode controller changes depending...
on the rate of change of error shown in the Fig.3. That is, when the error is large one might choose one control strategy and for sufficiently small error another control strategy. It is thus a discontinuous mode of operation. When the error is sufficiently small and remains small the control structure is not changed. It may be called the continuous mode of operation.

Fig. 3 Error Signal

VI. PROPOSED AUTOMATIC GENERATION CONTROL STRATEGY

As mentioned in the beginning of this section the control algorithm in the proposed approaches has two modes of operation, i.e. continuous and discontinuous. The control is based on the conventional techniques during the continuous mode. It is proposed that the control structure be switched during the discontinuous mode. The type of structure to be used during the discontinuous mode depends upon the particular problem and switching can be performed on a simple criterion such as rate of change of the error staying within a singular strip. A suitable control algorithm based on such variable structure control scheme is developed in Automatic Generation Control problem.

A. Discontinuous Mode

The control system will operate in this mode when the rate of change of the error signal, as shown in Fig.3 exceeds specified limit. In the discontinuous mode, the control should switch between two different control algorithms in the feedback loop until the rate of change of the error signal trajectory enters the singular strip permanently. The time at which these changes occur is determined in accordance with the current value of the derivative of the error signal. Based on the properties of the proportional and the integral control, the system response can be improved by employing a variable structure concept that combines useful properties of both the control action during the discontinuous mode. The control law employed during the transient period that is the discontinuous mode is switched between equations (3) and (4) depending upon the magnitude of the rate of change of the error signal.

\[ \Delta P_c(t) = -k_1 \int_{t_e}^{t} |ACE(t)| dt \]  

For \[ \left| \frac{d(ACE(t))}{dt} \right| > \varepsilon \]

\[ \Delta P_c(t) = -k_P \cdot ACE(t) \]  

Where \( ACE(t) \) is an error signal at a particular instant and \( \varepsilon = 0 \) is some constant indicating the specified limit of rate of change of the error signal.

and for \[ \left| \frac{d(ACE(t))}{dt} \right| \leq \varepsilon \]

\[ \Delta P_c(t) = -k_I \int ACE(t)dt \]  

Then if the parameters \( k_P, k_I \) and \( \varepsilon \) are suitably selected, one can ensure a high quality transient response. By choosing a suitable value of \( k_P \), one makes sure that speed of the system is high. Whenever the rate of change of error falls within the specified error bound \( \left| \frac{d(ACE(t))}{dt} \right| < \varepsilon \), the integrator starts accumulating the error. But if the error exceeds the bound the integrator resets to zero.

This continuous switching between the proportional and integral control strategies quickly brings the system to the continuous mode when \[ \left| \frac{d(ACE(t))}{dt} \right| < \varepsilon \).

B. Continuous Mode

When the rate of change of the error signal remains within the specified limit i.e. \[ \left| \frac{d(ACE(t))}{dt} \right| < \varepsilon \], the system will operate in the continuous mode. The integral control strategy is best able to meet the LFC requirements when the system enters the continuous mode. Thus the control law during the continuous mode would be

\[ \Delta P_c(t) = -k_I \int_{t_e}^{t} |ACE(t)| dt \]  

Where \( t_e < t \) is the time at which the error enters the region \( \left| \frac{d(ACE(t))}{dt} \right| < \varepsilon \) and remains in this region. The integral control will then eliminate the steady state error remaining in the system. The proposed control scheme is shown in Fig.4.

C. Performance with the proposed control

For the proposed control scheme, the control law is taken as
\[ \Delta P_d(t) = -\kappa_p [ACE_1(t)] \quad \text{for} \quad \frac{d(ACE_1(t))}{dt} > \varepsilon_1 \]

\[ \Delta P_d(t) = -\kappa_i [\int ACE_1(t) \, dt] \quad \text{for} \quad \frac{d(ACE_1(t))}{dt} \leq \varepsilon_1 \]

\[ \Delta P_{c2}(t) = -\kappa_{p2} [ACE_2(t)] \quad \text{for} \quad \frac{d(ACE_2(t))}{dt} > \varepsilon_2 \]

\[ \Delta P_{c2}(t) = -\kappa_{i2} [\int ACE_2(t) \, dt] \quad \text{for} \quad \frac{d(ACE_2(t))}{dt} \leq \varepsilon_2 \]

Where \( \kappa_{p1} = \kappa_{p2} = \kappa_p \), \( \kappa_{i1} = \kappa_{i2} = \kappa_i \), \( \varepsilon_1 = \varepsilon_2 = \varepsilon \) and \( \Delta P_{c1}(t) \) and \( \Delta P_{c2}(t) \) are the controls for area 1 and area 2 respectively.

VII. DESIGN PROCEDURE OF DUAL-MODE CONTROLLER

The main objective of the controller is to provide accurate actuating signal to the governor and respond first as well after small load perturbation. The accuracy of the signal depends on the switching and optimal value of \( \kappa_p \) and \( \kappa_i \). Routh-Hurwitz criteria is used to determine the range of \( \kappa_p \) and \( \kappa_i \) over which the system remains stable. While determining the stability zone, we neglect all non-linearities existing in the system such as governor deadband, GRC and governor valve position of the system as we need only the broad zone of \( \kappa_p \) and \( \kappa_i \). But we consider all the non-linearities at the time of searching optimum values of \( \kappa_p \) and \( \kappa_i \) by Hooke-Jeeve’s method within the broad stability zone of \( \kappa_p \) and \( \kappa_i \) determined by Routh array. The total designing work of the dual-mode controller [16] has been carried out by the following way:

Step 1:

Find out the overall transfer function (i.e. \( \frac{\Delta f}{\Delta P_D} \)) of the system considered. From this transfer function, derive the characteristic equation (denominator of the transfer function) of the system.

Step 2:

Investigate the upper and lower stability limit of the \( \kappa_p \) and \( \kappa_i \). Routh-Hurwitz criterion is used here to determine the stability limit of \( \kappa_p \) and \( \kappa_i \). In our proposed controller, either proportional or integral controller will act at a time depending on the control strategy. Therefore, we have to determine the stability zone of one parameter (either \( \kappa_p \) and \( \kappa_i \)) when the corresponding controller acts only. So we determine the stability zone of \( \kappa_p \) keeping \( \kappa_i \) equals to zero (i.e. no integral action) and the same for \( \kappa_i \).

Step 3:

Find out the optimum values of the parameters \( \kappa_p \) and \( \kappa_i \) as the controller performance depends upon the values of \( \kappa_p \) and \( \kappa_i \). The optimum values of the parameters \( \kappa_p \) and \( \kappa_i \), which minimize an array of different performance indices are easily and accurately computed using the Hooke-Jeeve’s optimization technique.

VIII. PERFORMANCE INDICES

The design of a control system is an attempt to meet a set of specifications, which define the overall performance of the system in terms of certain measurable quantities. A number of dynamic performance measures i.e. peak overshoot (\( P_a \)), rise time (\( t_r \)), peak time (\( t_p \)) and steady state error (\( e_{ss} \)), have been introduced for step and higher order inputs. These measures have to be satisfied simultaneously in design and hence the design necessarily becomes a trial and error procedure. If, however, a single performance index could be established on the basis of which one may describe the appropriateness of the system response, then the design procedure will become logical and straightforward [8,9]. Therefore performance index is a function of the variable system parameters. The other desirable features of a performance index are its sensitivity, i.e. its ability to clearly distinguish between an optimum and non-optimum system, its sensitivity to parameter variations and the ease of its analytical computation or its on-line analogical or digital determination [9].

The following performance indices in this study considered here [8,9] to measure the appropriateness of the system, are of the form,

a) Integrated Square of the error. It is defined as,

\[ ISE = \int_0^t (\Delta P_{tie}^2 \alpha \Delta f_1^2 + \gamma \Delta f_2^2) \, dt \]

b) Integrated time multiplied by absolute error (ITAE).

It is defined as,

\[ ITAE = \int_0^t (\Delta P_{tie} \alpha \Delta f_1 + \gamma \Delta f_2) \, dt \]

c) Integrated absolute error (IAE). It is defined as

\[ IAE = \int_0^t (\Delta P_{tie} \alpha \Delta f_1 + \gamma \Delta f_2) \, dt \]

Here \( \alpha \) and \( \gamma \) are the penalty factors for the frequency deviation in both areas. Both the values equal to 0.065 are considered here [6]. The responses of errors (i.e. \( \Delta P_{tie}, \Delta f_1 \) and \( \Delta f_2 \) ) improve with the accurate values of controller parameters, \( \kappa_p \) and \( \kappa_i \).

IX. RESULTS AND DISCUSSION

The simulation of proposed dual mode PI controller is carried out using MATLAB® SIMULATION TOOLBOX. To simplify the analysis, the two inter connected areas are considered identical. For comparative study between the VSS controller [1] and the proposed controller, the same values of the system parameters [7] are used as given in Table 1. The performance of the controller is investigates considering non-heat turbines only. The unit step input disturbance reveals useful information about the speed of response of the system. Therefore, a step load change is considered for evaluating the transient performance of the system.
The proposed control algorithm or switching scheme (SS) is simulated by using SIMULINK model as shown in Fig.5. The switching scheme given in Fig.5 works by switching between proportional controller and integral controller depending on the specified value, ε, of rate of change of the error signal. The optimum values of ε, κp, and κi are determined off-line. The optimum values of above parameters are determined by considering different performance indices.

**A. Nonreheat Turbine**

All the data from the Table 1 have been used here. Nonreheat turbine is considered first without any physical constraints and then with physical constraints.

**1) Nonreheat Turbine without Physical Constraints**

In this study, no physical constraints are imposed on the system variables while finding the system response after a load change. Two load changes are considered in area 1 to investigate the performance of the proposed controller.

- Case 1: A step load disturbance 0.005 p.u. in area 1
- Case 2: A step load disturbance 0.01 p.u. in area 1

Case 1 (Load change 0.005 p.u. in area 1):

The optimum values of ε, κp, and κi for nonreheat turbine without physical constraints at different performance indices are studied and results are shown in Table 2 to Table 4. Table 2 indicates the values of different time response parameters i.e. t_p (peak time), t_o (maximum overshoot) and t_s (settling time) of the response of frequency in area 1(Δf1) and optimum values of κp and κi at different ε values when ISE is considered as Performance index. Though the values of peak time and peak overshoot are almost same at different ε but settling time becomes minimum when ε is 0.004. The same investigation is carried out where performance indices are ITAE and IAE.

**TABLE I. INPUT SYSTEM PARAMETERS**

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>D1</td>
<td>5.33 x 10^-6 pu MW</td>
</tr>
<tr>
<td>R1</td>
<td>3 sec</td>
</tr>
<tr>
<td>P1</td>
<td>14 MW (area rated capacity)</td>
</tr>
<tr>
<td>Fmax</td>
<td>14 MW (line capacity)</td>
</tr>
<tr>
<td>T1</td>
<td>2.5 sec</td>
</tr>
<tr>
<td>R1 = 2.4 Hz/pu MW</td>
<td></td>
</tr>
<tr>
<td>T_e</td>
<td>0.08 sec</td>
</tr>
<tr>
<td>T_e = T_e = 0.3 sec</td>
<td></td>
</tr>
<tr>
<td>E</td>
<td>0.425</td>
</tr>
<tr>
<td>Kp</td>
<td>120 Hr/pu M W</td>
</tr>
</tbody>
</table>

**Fig. 5 Dual Mode Switching Scheme Simulated by the help of Simulation Toolbox**

<table>
<thead>
<tr>
<th>ε</th>
<th>Peak time (sec)</th>
<th>Peak overshoot (%)</th>
<th>Setting time (sec)</th>
<th>Optimum values of κp, κi</th>
<th>Performance Index</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.005</td>
<td>0.55</td>
<td>0.010555</td>
<td></td>
<td>0.14</td>
<td>0.77</td>
</tr>
<tr>
<td>0.004</td>
<td>0.55</td>
<td>0.010000</td>
<td></td>
<td>0.14</td>
<td>0.55</td>
</tr>
<tr>
<td>0.005</td>
<td>0.55</td>
<td>0.010000</td>
<td></td>
<td>0.18</td>
<td>0.64</td>
</tr>
</tbody>
</table>

**TABLE II. DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ISE**

**TABLE III. DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ITAE**

**TABLE IV. DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ITAE**
Fig. 6 Dynamic Response for Nonreheat Turbine at Load Change 0.005 p.u. in Area 1 Frequency Deviations area 1 and area 2 (b) Tie line Power Deviation (c) Deviations of Generated power area 1 and area 2 (d) Control Signal(area 1)

**TABLE V DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ISE**

<table>
<thead>
<tr>
<th>ε</th>
<th>Peak</th>
<th>Peak</th>
<th>Setting</th>
<th>Optimum</th>
<th>Performance</th>
</tr>
</thead>
<tbody>
<tr>
<td>time(hs)</td>
<td>overshoot</td>
<td>time(hs)</td>
<td>value of</td>
<td>Index</td>
<td></td>
</tr>
<tr>
<td>0.004</td>
<td>0.66</td>
<td>0.00182821</td>
<td>1355</td>
<td>375</td>
<td>0.6125</td>
</tr>
<tr>
<td>0.002</td>
<td>0.62</td>
<td>0.00166141</td>
<td>1450</td>
<td>370</td>
<td>0.3003</td>
</tr>
<tr>
<td>0.006</td>
<td>0.67</td>
<td>0.00169459</td>
<td>1390</td>
<td>370</td>
<td>0.1478</td>
</tr>
</tbody>
</table>

**TABLE VII DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ITAE.**

<table>
<thead>
<tr>
<th>ε</th>
<th>Peak</th>
<th>Peak</th>
<th>Setting</th>
<th>Optimum</th>
<th>Performance</th>
</tr>
</thead>
<tbody>
<tr>
<td>time(hs)</td>
<td>overshoot</td>
<td>time(hs)</td>
<td>value of</td>
<td>Index</td>
<td></td>
</tr>
<tr>
<td>0.004</td>
<td>0.6</td>
<td>0.00128178</td>
<td>9.55 sec</td>
<td>C103</td>
<td>18.25</td>
</tr>
<tr>
<td>0.006</td>
<td>0.6</td>
<td>0.00128178</td>
<td>9.55 sec</td>
<td>C103</td>
<td>18.25</td>
</tr>
</tbody>
</table>

Fig. 7 shows the dynamic responses of ΔP, ΔP, ΔP, ΔP, and ΔP and control signal (area 1) at optimum values of ε = 0.005, κ = 0.22 and κ = 0.8.

2) Nonreheat turbine with GRC

In the presence of Generation rate constraint, (10% per minute is considered) a step load change of 0.005 p.u. in area 1 is assumed. The optimum values of ε, κp and κi for the nonreheat turbine with GRC at different performance indices are studied. The optimum values of ε = 0.004 is found best and ISE gives better dynamic response as compared to IAE and ITAE. Table 8 shows the dynamic response parameters of frequency deviation in area 1 and optimal value of κp and κi at ISE. Fig. 8 shows the dynamic responses (ΔP, ΔP, ΔP, ΔP, and ΔP) and control signal with GRC for a step load change 0.005 p.u. in the area 1 with ε = 0.004, κp = 0.24 and κi = 0.8.

**TABLE VIII DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ITAE.**

<table>
<thead>
<tr>
<th>ε</th>
<th>Peak</th>
<th>Peak</th>
<th>Setting</th>
<th>Optimum</th>
<th>Performance</th>
</tr>
</thead>
<tbody>
<tr>
<td>time(hs)</td>
<td>overshoot</td>
<td>time(hs)</td>
<td>value of</td>
<td>Index</td>
<td></td>
</tr>
<tr>
<td>0.004</td>
<td>0.6</td>
<td>0.0011645</td>
<td>13.17</td>
<td>3.45</td>
<td>0.602</td>
</tr>
<tr>
<td>0.005</td>
<td>0.6</td>
<td>0.0011645</td>
<td>13.17</td>
<td>3.45</td>
<td>0.602</td>
</tr>
<tr>
<td>0.006</td>
<td>0.6</td>
<td>0.0011645</td>
<td>13.17</td>
<td>3.45</td>
<td>0.602</td>
</tr>
</tbody>
</table>

Table 9 compares the results obtained from the proposed controller and the same of Variable Structure Scheme (VSS) controller reported in reference [3]. It can be observed that great improvements in system performance have been obtained by using the proposed dual mode control scheme.

**TABLE IX COMPARISON OF PERFORMANCE FOR THE CASE OF NONREHEAT TURBINE WITH GENERATION RATE CONSTRAINT WITH VSS**

<table>
<thead>
<tr>
<th>κi</th>
<th>Setting</th>
<th>Max. deviation</th>
<th>κp</th>
<th>Setting</th>
<th>Max. deviation</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.005</td>
<td>0.0010</td>
<td>0.0010</td>
<td>0.005</td>
<td>0.0010</td>
<td>0.0010</td>
</tr>
</tbody>
</table>

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3) Nonreheat turbine with GRC and Governor Deadband

Similar simulation studies have been performed at nonreheat turbine with GRC and Governor Deadband. Governor Deadband is considered to avoid excessive operation of the Governor. The limiting value of governor deadband is specified as ±0.06%. Table 10 shows the time response parameters of frequency deviation in area 1(Δf1) for a load change 0.005 p.u. when ISE is considered as performance index and dynamic responses are shown in Fig.9.

By comparing the values of overshoot and settling time in Table 2, Table 8 and Table 10, it can be observed that the responses are deteriorating with the increase in the number of physical constraints. It is obvious because GRC and governor deadband are restricting the magnitude of input signal when the input violates the limit of GRC and deadband. As a result, the output of the signal from controller does not correspond to the actual input signal. The same observation can be drawn from the graphical representation in Fig.6, Fig.8 and Fig.9.

### TABLE X DIFFERENT VALUES OF TIME RESPONSE PARAMETERS AND OPTIMUM VALUES OF CONTROLLER PARAMETERS AT ISE

<table>
<thead>
<tr>
<th>ε</th>
<th>Peak overshoot (p.u.)</th>
<th>Peak overshoot (p.u.)</th>
<th>Settling time (Sec)</th>
<th>Optimum value of Ki</th>
<th>Performance index</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.000</td>
<td>0.60</td>
<td>0.0114858</td>
<td>12.00</td>
<td>0.080 0.80</td>
<td>3.2x10^{-6}</td>
</tr>
<tr>
<td>0.004</td>
<td>0.65</td>
<td>0.015461</td>
<td>10.45</td>
<td>0.060 0.80</td>
<td>2.6x10^{-6}</td>
</tr>
<tr>
<td>0.000</td>
<td>0.65</td>
<td>0.011485</td>
<td>13.00</td>
<td>0.060 0.80</td>
<td>2.2x10^{-6}</td>
</tr>
</tbody>
</table>

### X. CONCLUSIONS

A control algorithm based on the dual mode concept has been investigated for load frequency control of interconnected power systems. By properly selecting the control parameters of the Dual mode controller, the frequency deviations and the tie line power can effectively be controlled in the presence of generation rate constraint and Governor deadband. Hooke-Jeeves’s method is used for optimizing the control parameters. The proposed control concept gives better response in comparison to Variable Structure System (VSS). Moreover, VSS controller requires knowledge of all the state variables and thus practical realization of the controllers is more involved and expensive, requiring state estimators and inter area data transfer over long distances. Whereas, the proposed control algorithm is very simple in structure and easy to implement, as it requires only one variable i.e. rate of change of the area control error which is already available in the system.

### XI. APPENDIX

\[\Delta P_{g1} = \text{incremental generation change},\]
\[\Delta X_{g1} = \text{incremental governor valve position change} \]
\[\Delta P_{l1} = \text{incremental load demand change} \]
\[\Delta f_1 = \text{incremental frequency deviation} \]
\[\Delta P_{ci} = \text{incremental change in tie-line power} \]
\[\Delta P_{ci} = \text{incremental change in speed changer position} \]
\[f = \text{nominal system frequency} \]
\[I_1 = \text{inertia constant} \]
\[D_1 = \text{load frequency constant} \]
\[\left( K_{p} = \frac{1}{D_1}, T_p = \frac{2H_1}{fD_1} \right) \]
\[T_{\theta} = \text{synchronizing coefficient} \]
\[R_i = \text{speed regulation parameter} \]
\[T_{g1} = \text{governor time constant} \]
\[T_{n1} = \text{turbin time constant} \]
\[K_{r1}, T_{r1} = \text{reheat coefficient and reheat time constant} \]
\[T_{pi} = \text{Power System time constant} \]

The area control error (ACE) for the ith area is defined as
\[\text{ACE}_i = \Delta f_{ci} + B\Delta f_1 \quad \text{(A.1)}\]
Where, $B$, is the frequency bias constant. The conventional automatic generation controller has a linear integral control strategy of the form

$$\Delta P_c = -K_p \Delta f + B \Delta f$$ \hspace{2cm} (A.2)

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